

Professor: J.D. Wilson      Time available: 80 mins      Value: 20%***Instructions: Closed book exam. Please record your answers in the exam booklet. Pertinent data are at the back.*****Multi-choice** (20 x  $\frac{1}{2}\%$   $\rightarrow$  10%)

1. If  $x(t)$  is a stationary random signal with zero mean and unit standard deviation, the autocorrelation function for  $x$  is  $R(\xi) =$  \_\_\_\_\_

- (a)  $\overline{x(t) - x(t + \xi)}$
- (b)  $\overline{x^2(\xi)}$
- (c)  $\overline{x(t) x^{-1}(t + \xi)}$
- (d)  $\overline{x(t) x(t + \xi)}$       ✓✓
- (e)  $\sqrt{\overline{x(t) x(t + \xi)}}$

2. A random variable  $x$  is decomposed into the sum of its mean  $m_x$  and a deviation  $x'$ , ie.  $x = m_x + x'$ . The mean value  $E[x']$  of  $x'$  satisfies:

- (a)  $E[x'] = m_x$
- (b)  $E[x'] = s_x$ , the standard deviation of  $x$
- (c)  $E[x'] = 0$       ✓✓
- (d)  $E[x'] = s_x^2$ , the variance of  $x$
- (e) none of the above

3. The uncertainty due to random error, in a single measurement of temperature by a particular noisy (but unbiased) thermometer, is  $\delta T = 1^\circ \text{C}$ . If the true temperature is constant, and it is estimated by an average  $\bar{T}$  over a sample  $T_1, T_2, T_3 \dots T_N$  taken with this instrument, then if  $N = 25$ , the uncertainty in  $\bar{T}$  is \_\_\_\_\_  $^\circ\text{C}$

- (a) 0.04
- (b) 0.2      ✓✓
- (c) 0.5
- (d) 2.5
- (e) 5

4. Suppose temperature is fluctuating about its mean value with standard deviation  $\sigma_T = 3^\circ \text{ C}$ , and that  $\bar{T}$  is an average over  $N = 25$  independent samples, taken with an unbiased, noise-free sensor able to follow all fluctuations ( $T_{meas} = T_{true}$ ). Then with 95% probability  $\bar{T}$  is no further than  $\epsilon = \underline{\hspace{2cm}}$   $^\circ \text{ C}$  from the true mean
- (a) 1/5  
 (b) 2/5  
 (c) 3/5  
 (d) 6/5    ✓✓  
 (e) 6/25
5. A cylindrical chamber containing volume  $V$  and having basal area  $A$  is placed over the soil at time  $t = 0$ . The air inside the chamber is continuously mixed by a fan, and the concentration ( $C$ ,  $\text{kg m}^{-3}$ ) of a particular gas escaping from the soil and accumulating inside the chamber is observed to increase over the next  $T$  [s] by amount  $\Delta C$ . The average rate of release of the gas, per unit ground area, over the period  $T$  was  $\underline{\hspace{2cm}}$
- (a)  $\frac{V}{A} \frac{\Delta C}{T}$     ✓✓  
 (b)  $V \frac{\Delta C}{T}$   
 (c)  $\frac{\Delta C}{T}$   
 (d)  $\frac{A}{V} \Delta C$   
 (e)  $TV \frac{\Delta C}{A}$
6. Suppose it is known that (on theoretical grounds) the current output  $I$  from a certain electromagnetic absorption hygrometer varies with absolute humidity  $\rho_v$  according to  $\log_e I \propto -\rho_v$ . A two-point calibration based on the observations of the table below indicates the calibration law is  $\underline{\hspace{2cm}}$

$I$ [mA]	$\rho_v$ [ $\text{g m}^{-3}$ ]
1.00	0.0
0.05	10.0

- (a)  $\rho_v = -0.30 \log_e I$   
 (b)  $\rho_v = -0.095 \log_e I$   
 (c)  $\rho_v = -10.5 \log_e I$   
 (d)  $\rho_v = -3.33 \log_e I$     ✓✓  
 (e)  $\rho_v = 0.30 (\log_e I)^{-1}$

7. For many simple instruments the input-output relationship can be represented

$$y(t) = \int_{\xi=0}^{\infty} x(t - \xi) \exp(-\xi/\tau) d\xi$$

(this is the I/O characteristic of a linear, 1<sup>st</sup>-order system). The input signal is \_\_\_\_\_ and the “system weighting function” is \_\_\_\_\_

- (a)  $y; x$
- (b)  $x; y$
- (c)  $x; \tau$
- (d)  $y; \exp(-\xi/\tau)$
- (e)  $x; \exp(-\xi/\tau)$  ✓✓

8. An example of an environmental sensor having the above temporal response characteristic is \_\_\_\_\_

- (a) a wind vane
- (b) a sonic anemometer
- (c) an ordinary thermometer (eg. mercury-in-glass) ✓✓
- (d) a cup anemometer
- (e) none of the above

9. Let  $\dot{\theta}$  be the rotation rate of a cup anemometer, and let  $I$  be the moment of inertia of the cup-assembly. The statement that  $I d\dot{\theta}/dt = 0$  implies \_\_\_\_\_

- (a) there is no wind
- (b) the cups are not rotating
- (c) the cups are in a state of steady rotation
- (d) the angular acceleration of the cup assembly is zero
- (e) both (c) and (d) apply ✓✓

10. The provision of air bearings for a propellor anemometer overcomes which error?

- (a) inertial error
- (b) cosine error
- (c) non-linearity at high speeds
- (d) threshold error ✓✓
- (e) both (a) and (b)

11. The “pitch angle” ( $\theta$ ) of each blade of a propellor anemometer varies with distance  $r$  from the axis of rotation,  $\theta = \theta(r)$ . This is arranged so that
- (a) at the equilibrium rotation rate, angle of incidence of the *relative* wind on the blade vanishes at all points along the blades ✓✓
  - (b) calibration will be independent of air (or fluid) density
  - (c) inertia of the anemometer is minimized
  - (d) cosine error is minimized
  - (e) none of the above
12. A propellor velocity-sensor has a sensitivity of  $10 \text{ [mV (m s}^{-1}\text{)}^{-1}\text{]}$ . It is placed obliquely in a uniform stream, at an angle of  $30^\circ$  with respect to the flow. If its output is  $20 \text{ mV}$ , then the velocity of the stream, assuming an ideal cosine response, is \_\_\_\_\_  $\text{[m s}^{-1}\text{]}$
- (a)  $20/\cos(30)$
  - (b)  $20 \cos(30)$
  - (c)  $20/(10 \cos(30))$  ✓✓
  - (d)  $20 \tan(30)$
  - (e)  $\sqrt{20^2 + \cos^2(30)}$

13. Suppose the random variable  $x$  has p.d.f.  $f(x) = \begin{cases} 0 & x < -\frac{1}{2} \\ \alpha(1-x) & -\frac{1}{2} \leq x \leq \frac{1}{2} \\ 0 & x > \frac{1}{2} \end{cases}$
- In order that  $f(x)$  should be a p.d.f.,  $\alpha =$  \_\_\_\_\_ (Hint: you can get the answer either by geometric reasoning, or by doing the Calculus)

- (a)  $1/x$
  - (b)  $x$
  - (c)  $x^2$
  - (d)  $1$  ✓✓
  - (e)  $0$
14. The variable  $x$  has been measured to have the value  $X \pm \epsilon_x$ , where  $\epsilon_x$  is the absolute uncertainty. The absolute uncertainty in the derived variable  $y = (2/x) + 1$  is \_\_\_\_\_
- (a)  $2\epsilon_x$
  - (b)  $2/\epsilon_x$
  - (c)  $2/(1 + \epsilon_x)$
  - (d)  $2\epsilon_x/X^2$  ✓✓
  - (e)  $X/\epsilon_x$

15. The units of spectral radiative intensity  $I_\nu$  are \_\_\_\_\_
- (a)  $\text{W m}^{-2} \mu\text{m}^{-1}$
  - (b)  $\text{J s}^{-1} \text{m}^{-2} \text{steradian}^{-1}$
  - (c)  $\text{W s}^{-1} \text{m}^{-2} \mu\text{m}^{-1}$
  - (d)  $\text{J s}^{-1} \text{m}^{-2} \text{steradian}^{-1}$
  - (e)  $\text{J s}^{-1} \text{m}^{-2} \text{steradian}^{-1} \mu\text{m}^{-1}$  ✓✓
16. In the longwave band, absorbtivity  $a$  is equal to emissivity  $\epsilon$ . Suppose a perfect radiometer is placed in an isothermal room (temperature  $T$ ) and, facing down at a plane surface whose emissivity is  $\epsilon < 1$ , measures the upwelling hemispheric longwave radiant energy flux density  $L \uparrow$ . The radiometer will detect a flux  $L \uparrow =$  \_\_\_\_\_
- (a)  $\epsilon\sigma T^4$
  - (b)  $(1 - \epsilon)\sigma T^4$
  - (c)  $(1 - a)\sigma T^4 + \epsilon\sigma T^4$
  - (d)  $\sigma T^4$
  - (e) (c) and (d) are equivalent, and correct ✓✓
17. A sphere of radius  $R$  is held suspended inside a closed, evacuated chamber. The entire system is allowed to come to an isothermal equilibrium at  $0^\circ\text{C}$ . The net radiative energy flux density  $Q^*$  [ $\text{W m}^{-2}$ ] at the surface of the sphere is \_\_\_\_\_
- (a) zero ✓✓
  - (b)  $\sigma 273^4$
  - (c)  $\sigma 273^4 \pi R^2$
  - (d)  $\sigma 273^4 4\pi R^2$
  - (e)  $\sigma 273^4 \frac{4}{3}\pi R^3$
18. The allwave absorbtivity of a surface exposed to solar and terrestrial radiation can be written  $\alpha = (aK + \epsilon L) / (K + L)$  where  $K, L$  are the incident shortwave and longwave radiant energy fluxes, and  $a$  is the \_\_\_\_\_ of the surface
- (a) shortwave reflectivity
  - (b) shortwave absorbtivity ✓✓
  - (c) shortwave transmissivity
  - (d) emissivity
  - (e) net radiation

19. A simple scientific model of the net radiometer (with isolating domes) suggests the calibration relationship  $\alpha Q^* = (4\epsilon\sigma T^3 + 2k/d)(T_t - T_b)$  where  $T_t, T_b$  are the temperatures of the upper and lower surfaces (sensed by a thermopile),  $\alpha, \epsilon$  are respectively the allwave and longwave absorptivities,  $d$  is the separation of the planes of thermocouple junctions, and  $k$  is the conductivity of the slab between upper and lower surfaces. Suppose that rather than being separated from each other by a (somewhat) thermally conductive matrix, the upper and lower planes of thermocouple junctions were thermally isolated ( $k = 0$ ). Where for finite  $k$  (which ensures  $4\epsilon\sigma T^3 \ll 2k/d$ ) one had had a 1:1 (unique) relationship between  $T_t - T_b$  (thermopile measurement) and the inferred environmental variable ( $Q^*$ ), introducing thermal isolation between the junctions would \_\_\_\_\_ the relationship between  $T_t - T_b$  and  $Q^*$ .

- (a) enhance
- (b) render more accurate
- (c) render more precise
- (d) render ambiguous ✓✓
- (e) reverse

20. The energy balance of a wet-bulb thermometer, operating ideally at steady state, reduces to \_\_\_\_\_

- (a)  $C \frac{dT}{dt} = 0 = A(Q^* + Q_H + Q_E) + 0$
- (b)  $C \frac{dT}{dt} = A(0 + Q_H + Q_E) + P$
- (c)  $C \frac{dT}{dt} = 0 = P$
- (d)  $|Q_H| = |Q_E|$  ✓✓
- (e)  $C \frac{dT}{dt} = A(Q_H + Q_E)$

## Short Answer (10 %)

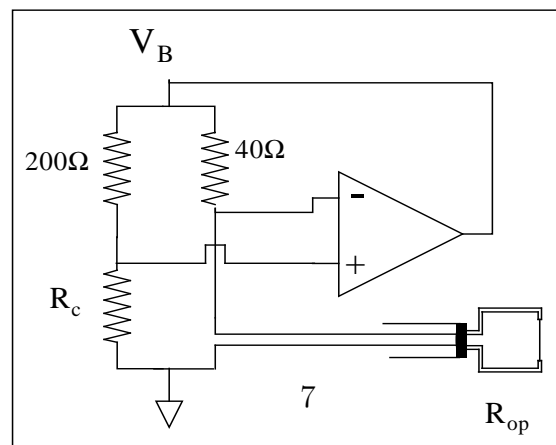
Answer **two** questions from this section. Give diagrams where appropriate. Justify any assumptions or simplifications you make. (13 April 2005: Answers given at back)

1. You have just bought a cup of coffee from Java-Jive, and you have left your cup, which we shall treat as a styrofoam (conductivity  $k = 0.025 \text{ W m}^{-1} \text{ K}^{-1}$ ) cylinder of mean diameter  $d = 6 \text{ cm}$ , height  $h = 10 \text{ cm}$  and wall thickness  $d^* = 2 \text{ mm}$ , sitting freely exposed on a bench outside to a wind of speed  $U = 1 \text{ m s}^{-1}$  and temperature  $T_a = 20^\circ\text{C}$  (assume air density  $\rho_a = 1.1 \text{ kg m}^{-3}$ ). The interior temperature  $T_i$  can be assumed to be well-mixed (uniform), and at the instant you sat your cup down  $T_i = 85^\circ\text{C}$ .

Derive a formula for the surface temperature  $T_w(t)$  of the outside of the cup, under the approximation that heat is lost down a transfer pathway  $T_i \rightarrow T_w \rightarrow T_a$  under the control of two resistances  $R_{iw} \equiv d^*/k$  (across the styrofoam) and  $R_{wa} = r_H/(\rho_a c_{pa})$  (from outer surface to bulk airstream), where  $r_H [\text{s m}^{-1}]$  is the conventional convective heat transfer resistance appearing in the Ohm's Law analogy (see data at back; assume fully forced convection). The two resistances are configured in series, and a constant "current" (sensible heat flux  $Q_H$ ) flows through them.

From your formula, compute the surface temperature  $T_w$  of the cup at  $t = 0$  and at  $t = 15 \text{ min}$ .

2. A cylindrical hot-film anemometer has a "cold" resistance of  $R_0 = 6\Omega$  at temperature  $T_0 = 6^\circ \text{C}$ , and its resistance vs. temperature calibration is  $R(T) = R_0[1 + \alpha(T - T_0)]$ , where  $\alpha = 0.0018 [\text{K}^{-1}]$ .
  - calculate the required operating resistance  $R_{op}$  if the operating temperature  $T_{op}$  is to be  $300^\circ\text{C}$
  - calculate the required value of the control resistor  $R_c$  to ensure balance of the bridge circuit shown below
  - The hot-film has diameter  $d = 0.2 \text{ mm}$ . Assuming perfect balance of the bridge in an airstream of velocity  $U = 5 \text{ m s}^{-1}$  having temperature  $T_a = 20^\circ\text{C}$  and density  $\rho = 1.1 \text{ kg m}^{-3}$ , estimate the Nusselt number for convective heat loss and thence the required rate ( $P$ ) of power dissipation in the sensor to balance convective cooling. Deduce the heating current ( $i$ ) through the sensor, and the bridge voltage  $V_B$ .



3. Derive a formula for the rate of heat-loss [W] from the bare, exposed fist (sphere of diameter  $d = 10$  cm, approximated as being at temperature  $T_{sk}$ ) of a gloveless hang-glider pilot, who is at an altitude of about 7000' ASL where air pressure and temperature are about  $(p, T_a) = (80$  kPa,  $-10^\circ$  C), and who is flying at speed  $U = 10$  m s $^{-1}$  (about 20 mph). Evaluate your solution for the case that  $T_{sk} = 10^\circ$ C. Explain in physical terms, perhaps making reference to the “half bridge” (Fig. 1), what controls the skin temperature  $T_{sk}$ .

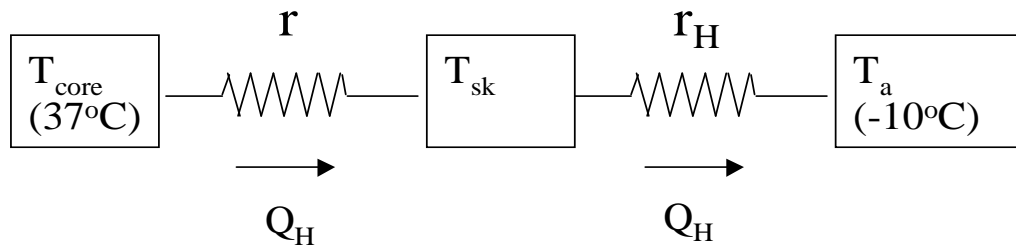


Figure 1: Resistor network model for factors determining skin temperature.



## Data:

- Kinematic viscosity of air:  $\nu \approx 1.5 \times 10^{-5} \text{ [m}^2 \text{ s}^{-1}\text{]}$
- Thermal diffusivity<sup>1</sup> of air:  $\kappa \equiv D_H \approx 2.1 \times 10^{-5} \text{ [m}^2 \text{ s}^{-1}\text{]}$
- Specific heat capacity of air at constant pressure:  $c_{pa} \approx 1000 \text{ [J kg}^{-1}\text{K}^{-1}\text{]}$
- Ideal gas law for air:  $P = \rho_a R_d T$  ( $R_d = 287 \text{ J kg}^{-1} \text{ K}^{-1}$ )
- Stefan-Boltzmann constant  $\sigma = 5.67 \times 10^{-8} \text{ W m}^{-2} \text{ K}^{-4}$
- $Q_H = k \frac{\Delta T}{\Delta x}$

Fourier's Law of conduction for the heat flux resulting from a temperature gradient of strength  $\Delta T/\Delta x$ , where  $k \text{ [W m}^{-1} \text{ K}^{-1}\text{]}$  is the thermal conductivity

- $Q_H = \rho c_p \frac{T_1 - T_2}{r_H}$

Ohm's law model for sensible heat exchange by bulk convection/conduction to/from a body to a fluid.

- $r_H = \frac{d}{D_H N_u} \text{ [s m}^{-1}\text{]}$

Relationship between heat transfer resistance  $r_H$  and the Nusselt number.

- $N_u = \begin{cases} 0.32 + 0.51 R_e^{0.52} & \text{if } 10^{-1} \leq R_e \leq 10^3 \\ 0.24 R_e^{0.6} & \text{if } 10^3 \leq R_e \leq 5 \times 10^4 \end{cases}$

Nusselt number versus Reynolds number ( $R_e = Ud/\nu$ ) for a cylinder (diameter  $d$ ) in a current of air of speed  $U$  (forced convection).

- $N_u = \begin{cases} 2 + 0.54 R_e^{0.5} & \text{if } 0 \leq R_e \leq 3 \times 10^2 \\ 0.34 R_e^{0.6} & \text{if } 5 \times 10^1 \leq R_e \leq 1.5 \times 10^5 \end{cases}$

Nusselt number versus Reynolds number ( $R_e = Ud/\nu$ ) for a sphere (diameter  $d$ ) in a current of air of speed  $U$  (forced convection).

- $C \frac{dT}{dt} = A ( Q^* + Q_H + Q_E ) + P$

Energy balance for a thermometer ( $A$  the surface area,  $C$  the bulk heat capacity,  $P$  internal heat production or consumption, other terms conventional).

---

<sup>1</sup>Symbols  $\kappa, D_H$  are both used for this quantity.

# Answers to short-answer questions

No penalty for cumulative errors (ie. an error early in the calculation counts only once). Also, no penalty if (eg.) you took the  $N_u(R_e)$  formula for a cylinder instead of a sphere, because the information was laid out on the exam in a way that made this an easy mistake to make.

1. The coffee cooling question. This was harder than I realized when I posed it; it was marked by assigning 1 per significant step towards solution. Note that in the “live” exam, the formula for  $R_{iw}$  was given incorrectly as  $R_{iw} \equiv k/d^*$ , which has units  $[\text{W m}^{-2} \text{K}^{-1}]$ . However clearly, in order to have the correct units in a heat transfer model of form  $Q_H [\text{W m}^{-2}] = \Delta T/R$ , it is  $1/R$  that must have units of  $[\text{W m}^{-2} \text{K}^{-1}]$ .

- Give a diagram of the two resistors in series, with “voltages”  $T_i$ ,  $T_w$ ,  $T_a$  controlling the current ( $Q_H$ ) of heat (the heat transfer diagram is the same in principle as that given in Question 3 for heat loss from an exposed hand; only the labeling differs). Note that the voltage at the bottom of the pathway,  $T_a$ , is analogous to ‘ground’ in an electrical circuit
- Then apply the voltage divider formula,  $T_w = T_a + \alpha (T_i - T_a)$  where  $\alpha = R_{wa}/(R_{wa} + R_{iw})$ . Determine the two resistances, to get  $\alpha$ :
- The resistance across the wall of the cup is easy,  $R_{iw} = d^*/k = 0.08 \text{ K W}^{-1} \text{ m}^2$ . To get the aerodynamic resistance  $R_{wa}$ :  $R_e = 4000 \rightarrow N_u = 0.24R_e^{0.6} = 34.8 \rightarrow r_H = 82 \text{ s m}^{-1} \rightarrow R_{wa} = 0.075 \text{ K W}^{-1} \text{ m}^2$ . Hence,  $\alpha = 0.48$
- Thus at  $t = 0$ ,  $T_w = 20 + 0.48 * (85 - 20) = 51^\circ \text{ C}$
- **Because the remainder of the problem requires information not given, I marked such that you could get 5/5 if you got this far without error.** For your interest, the balance of the calculation goes as follows:
- The coffee will cool according to

$$C \frac{dT_i}{dt} = A (T_i(t) - T_a) / (R_{iw} + R_{wa}) \quad (2)$$

where  $C = \text{J kg}^{-1} \text{K}^{-1}$  is the bulk heat capacity of the coffee, and  $A = \pi dh + 2 \pi (d/2)^2 = 0.0245 \text{ m}^2$ . Then the time constant for cooling is

$$\tau = \frac{C (R_{iw} + R_{wa})}{A} \quad (3)$$

- To evaluate  $\tau$  I should have given you the information that

$$C = 4186 \rho_w \pi (d/2)^2 h = 1184 \text{ J kg}^{-1} \text{K}^{-1} \quad (4)$$

(where  $4186 \text{ J kg}^{-1} \text{K}^{-1}$  is the specific heat capacity of water). The result is that  $\tau = 6900 \text{ s}$ , which does seem a little too long.

- and since I didn’t give you the formula you could hardly have been expected to guess that

$$T_i(t) = 20 (1 - e^{-t/\tau}) + 85 e^{-t/\tau} \quad (5)$$

and hence deduce that

$$T_i(900\text{s}) = 77 \text{ C} \quad (6)$$

2. Hot film anemometer calculations. Marked by subtracting 1/2 per significant mistake.

- $R_{op} = 9.175\Omega$
- $40R_c = 200R_{op} \rightarrow R_c = 45.88\Omega$
- $R_e = 66.7 \rightarrow N_u = 4.85 \rightarrow r_H = 1.96 \text{ s m}^{-1}$
- $Q_H = \rho c_p (T_{op} - T_a)/r_H = 1.51 \times 10^5 \text{ W m}^{-2} \rightarrow P = (\pi d \ell) Q_H$ , where (my slip-up)  $\ell$  was not stated
- $P = i^2 R_{op} \rightarrow i = \sqrt{\pi d \ell Q_H / R_{op}}$
- $V_B = i(R_{op} + 40)$

3. Compute the rate of heat loss from a hand modeled as a sphere. Marked by subtracting 1/2 per significant mistake.

- The rate of heat loss is  $P = A Q_H$
- surface area  $A = 4\pi(d/2)^2 = 0.0314 \text{ m}^2$
- sensible heat flux density  $Q_H = \rho c_p (T_{sk} - T_a)/r_H$
- $\rho = p/RT = 1.06 \text{ kg m}^{-3}$
- $R_e = 6.67 \times 10^4 \rightarrow N_u = 267 \rightarrow r_H = 17.8 \text{ s m}^{-1}$
- substituting,  $P = 37 \text{ W}$
- skin temperature is controlled by the relative values of  $r, r_H$  for according to this model

$$T_{sk} = T_a + (T_{core} - T_a) \frac{r_H}{r_H + r} \quad (7)$$

Note that the resistance  $r$  is controlled by internal (bodily) properties